



Extraction and purification of metabolites from microalgae: some insights in choice and ecodesign of processes

Pr Luc Marchal

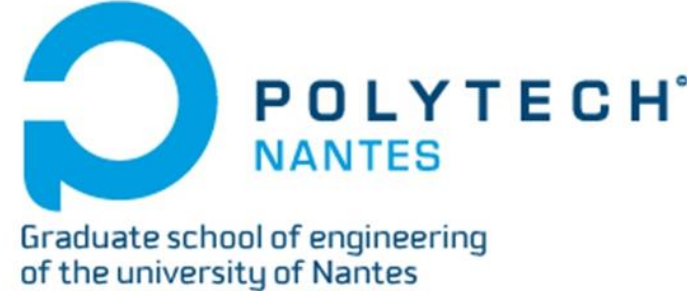
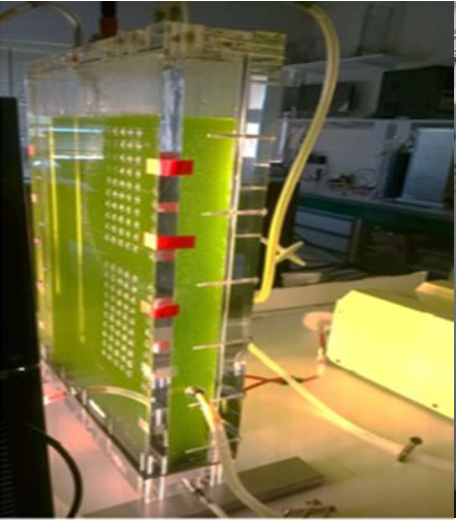
Head of Process and Bioprocess Engineering dpt (Polytech Nantes)

Scientific ref of CPC Engineering Business Unit of Capacités SAS

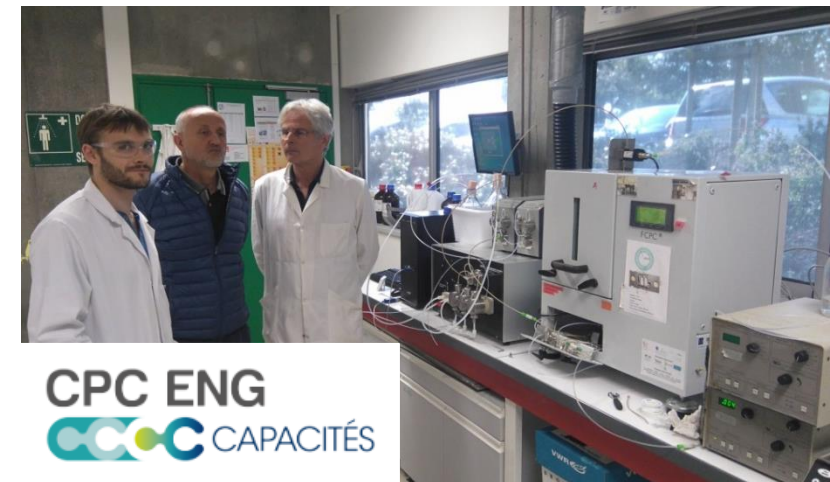
Biorefinery team of GEPEA Lab

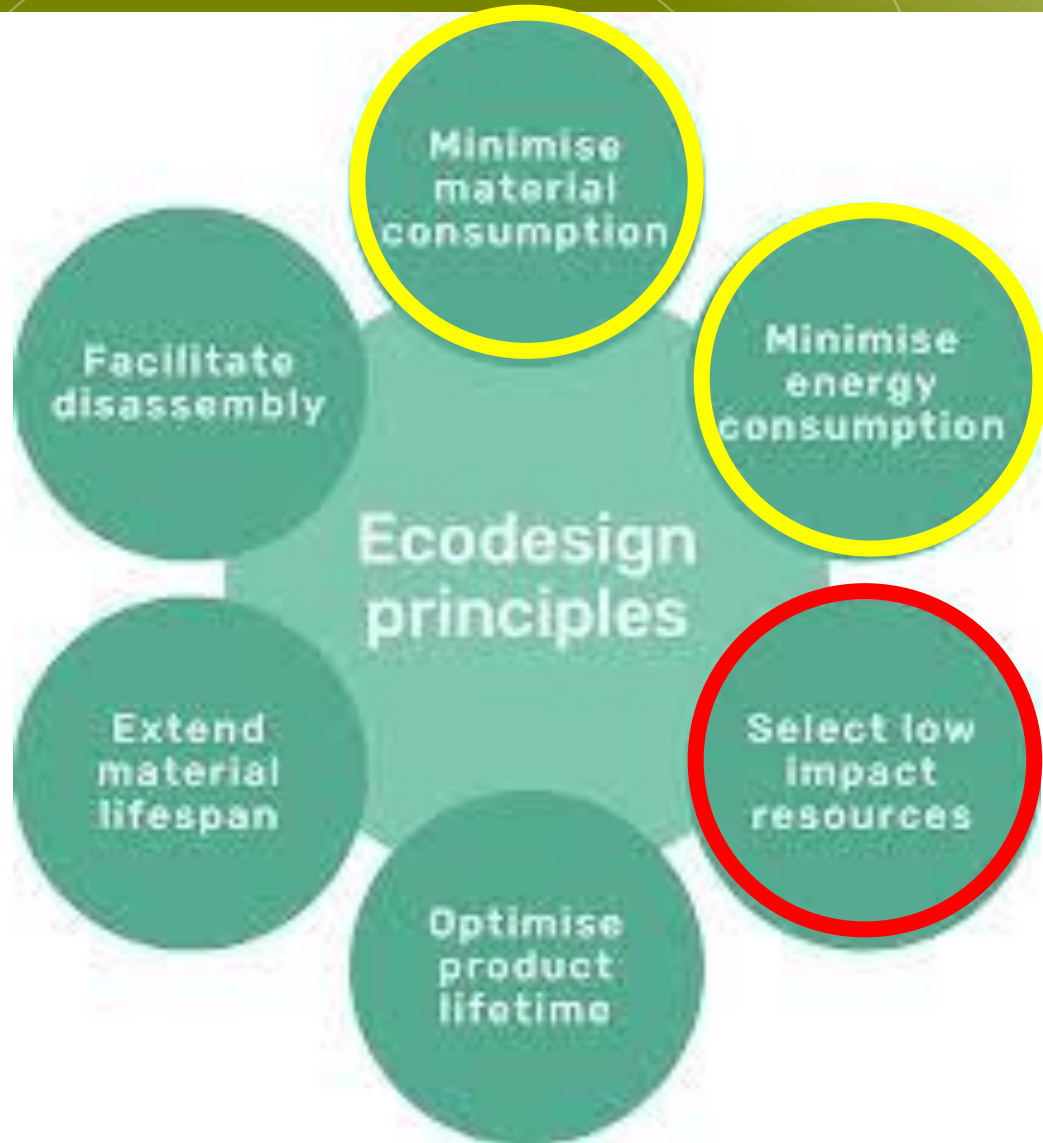
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Bioprocess Applied to Microalgae team Up-stream – Mid-stream – Down-stream



- ➔ Photobioreactor engineering
- ➔ Process integration (biorefinery)
- ➔ Wet biomass fractionation
 - Mechanical cell disruption
 - Membrane separation
 - Liquid-liquid extraction
 - Centrifugal Partition Chromatography
 - Scale-up





→ microalgae are identified as low impact renewable resources

→ take care of other resources (process facilities)

→ huge impact on BIOPROCESSES

(1 of the 10 bottlenecks)

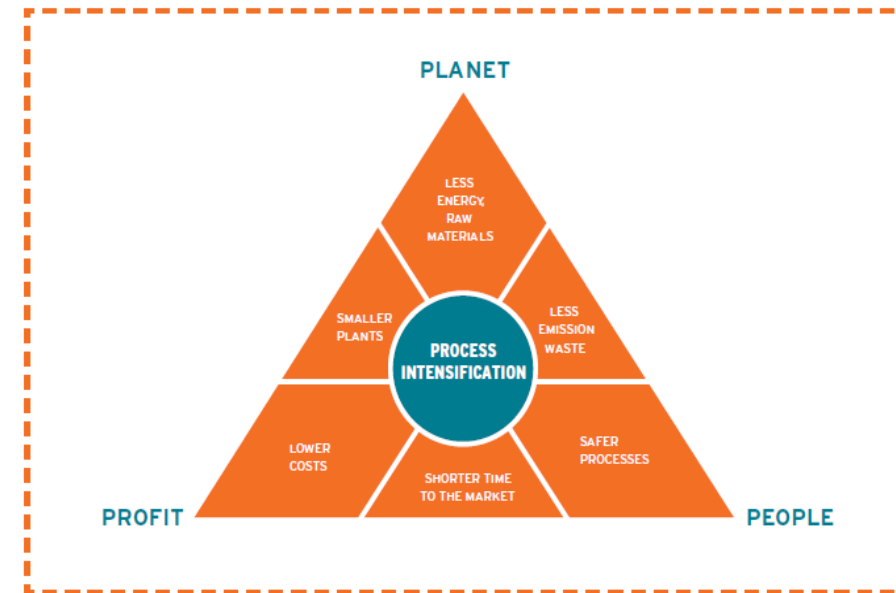
- choice (*technologies*)

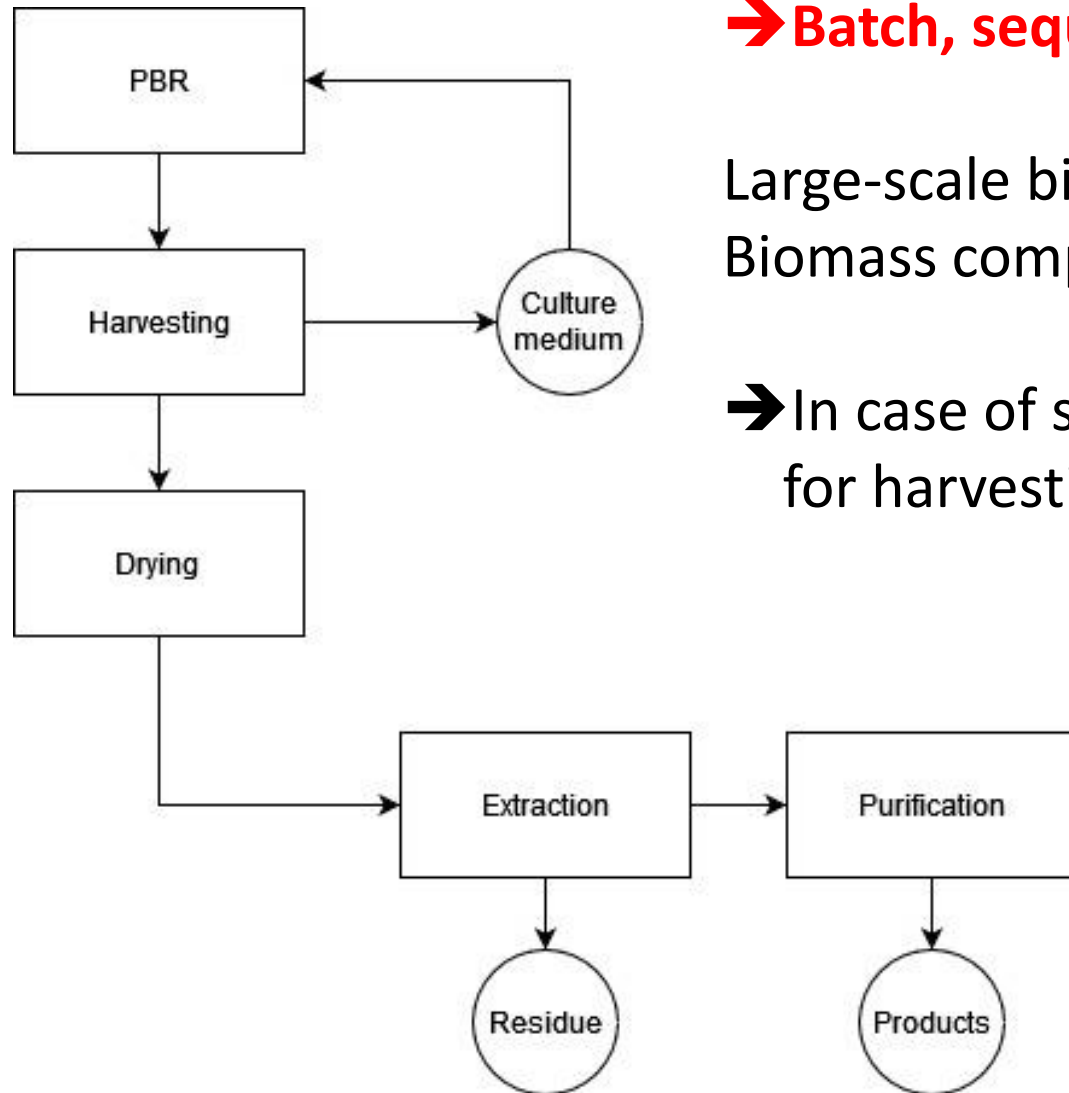
- design (*innovation, intensification, hybridation, integration, recycling*)

- development (*mass and energy consumption*)

3 approaches for microalgae DSP eco-design :

- Following the biological rhythm
batch, continuous or sequential ?
- Manage the water
dry or wet processing ?
- Extraction/Purification without solvent
alternatives, green solvents



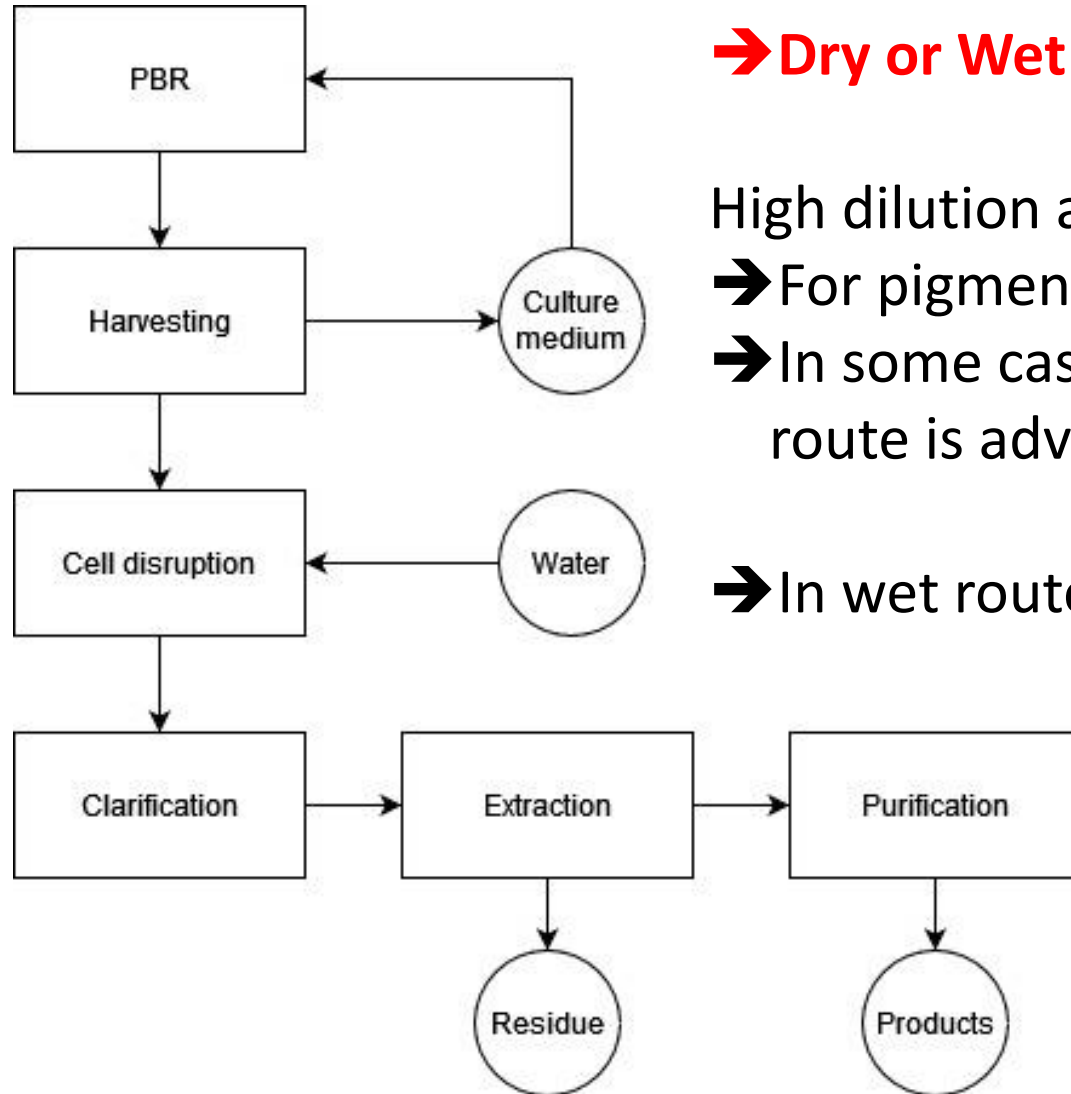


→ Batch, sequential or continuous process ?

Large-scale biomass production in solar conditions
Biomass composition, density... depend on the night/day time

→ In case of sequential mode, is there a right period for harvesting and processing ?





→ Dry or Wet processing ?

High dilution at PBR outlet (<1% dw)

→ For pigments extraction a dry route is convenient (*higher value*)

→ In some cases (soluble protein fractions, EPS, biodiesel) wet route is advantageous

→ In wet route, **cell disruption** is the controlling step

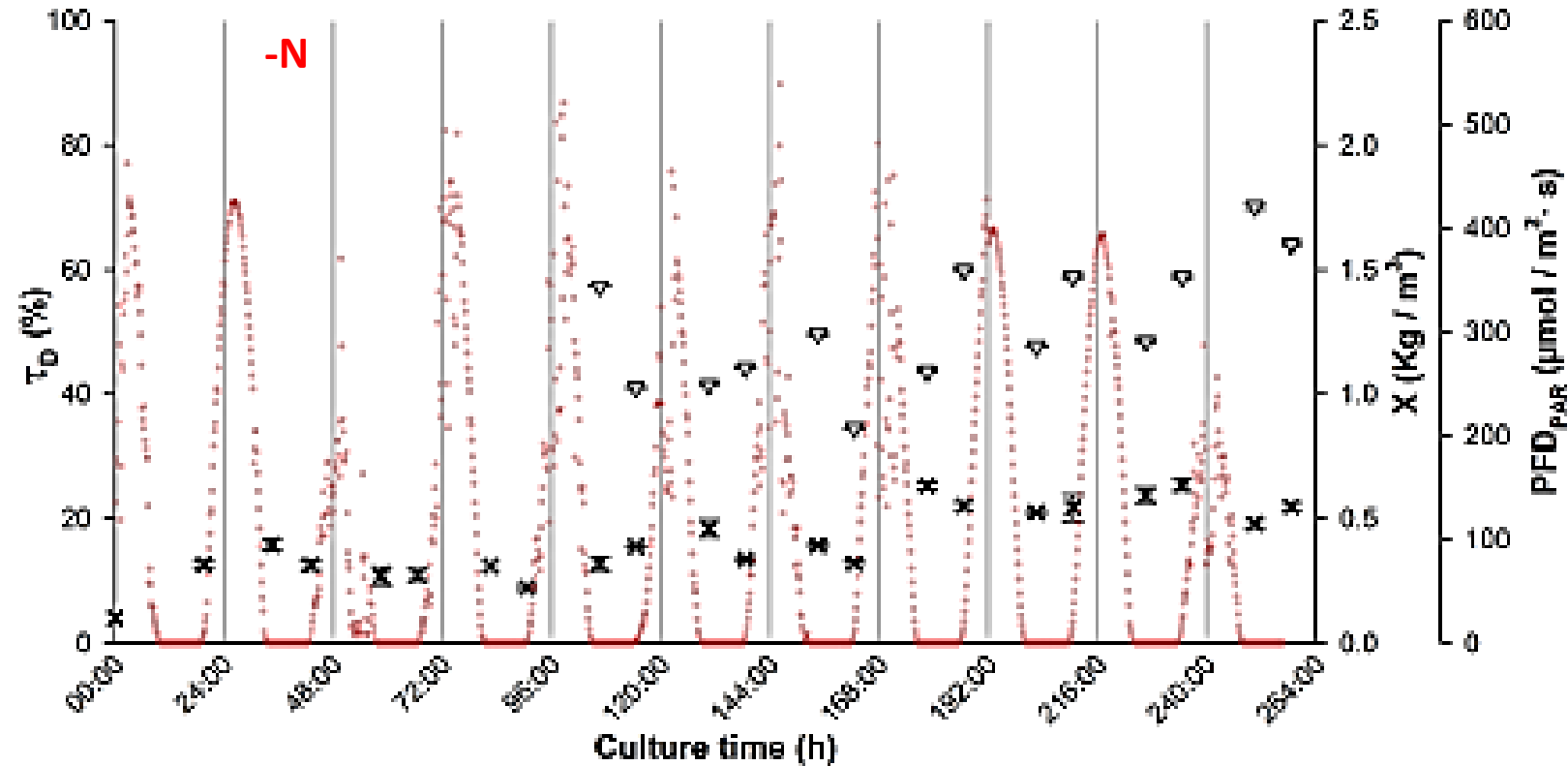


SEQUENTIAL PROCESS, INTEGRATION and ENERGY MINIMUM

Vladimir Heredia (2020)



Nannochloropsis oceanica



(c) Depleted culture

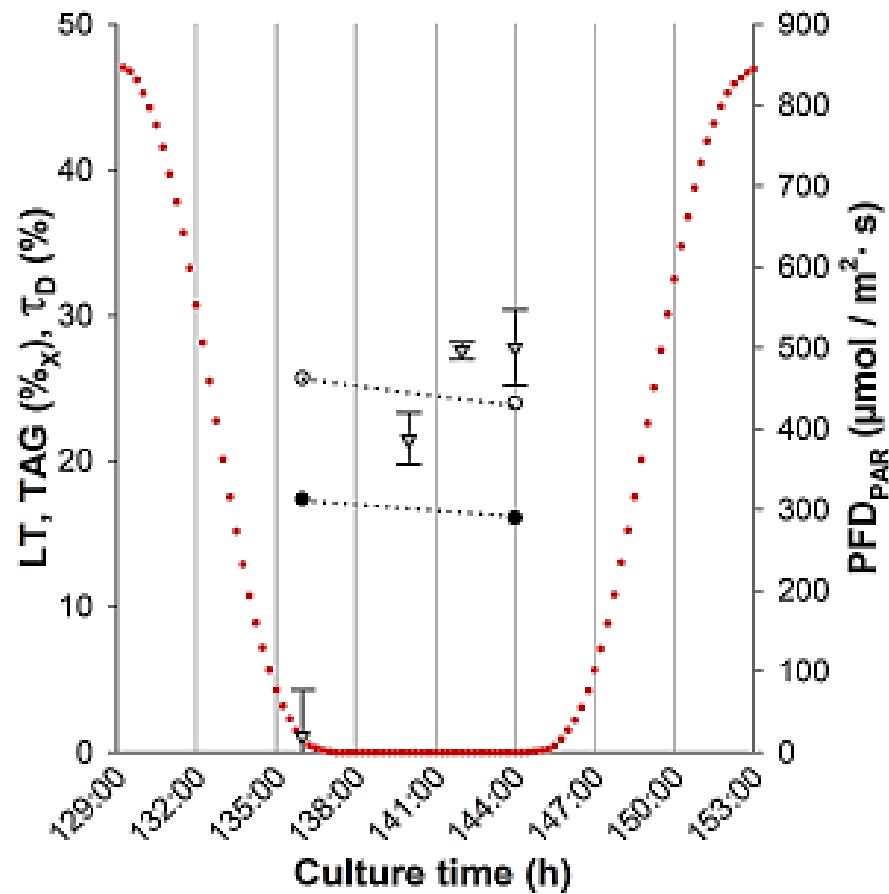


SEQUENTIAL PROCESS, INTEGRATION and ENERGY MINIMUM

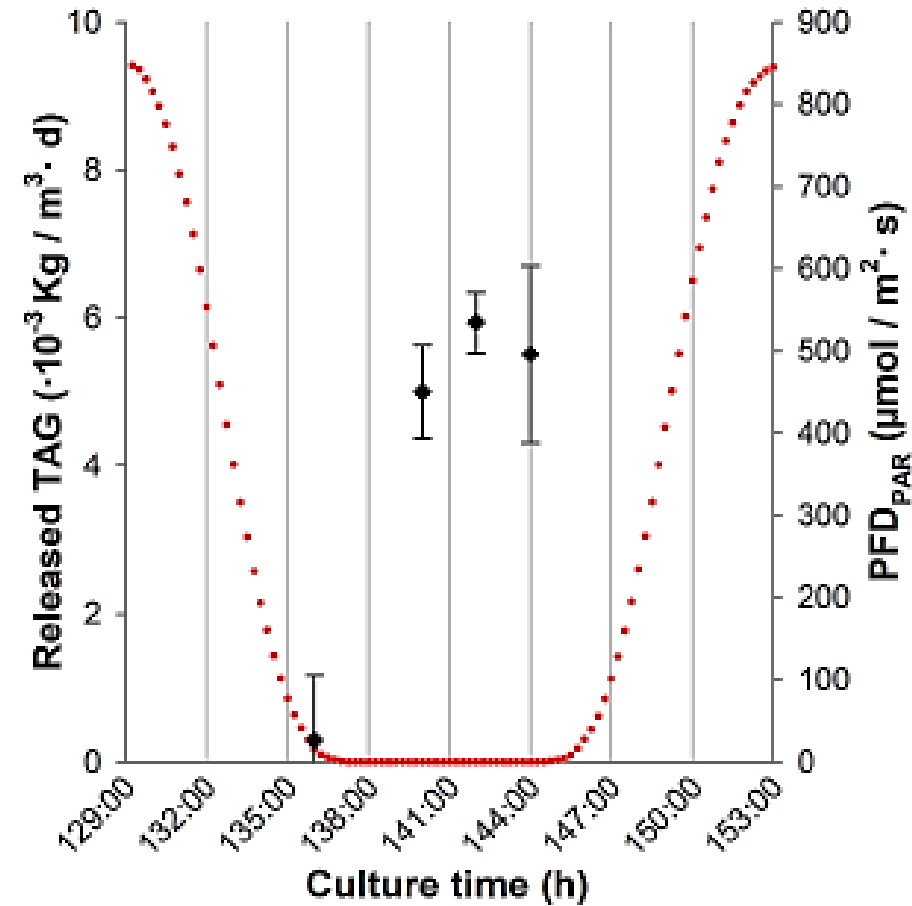
Vladimir Heredia

Nannochloropsis oceanica

Best harvesting period 5h after the end of de day



(a) τ_D , TFA, TAG



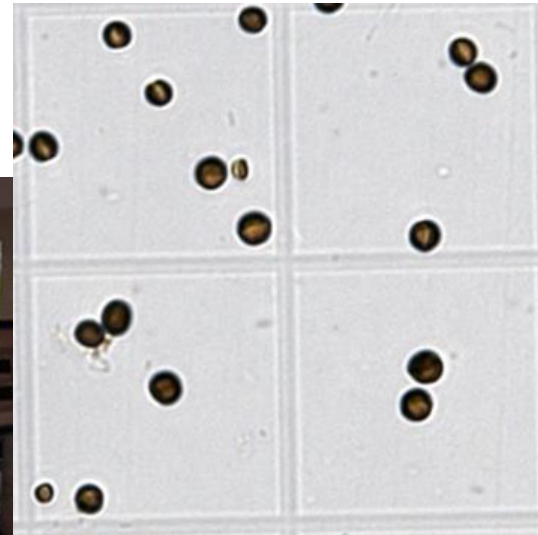
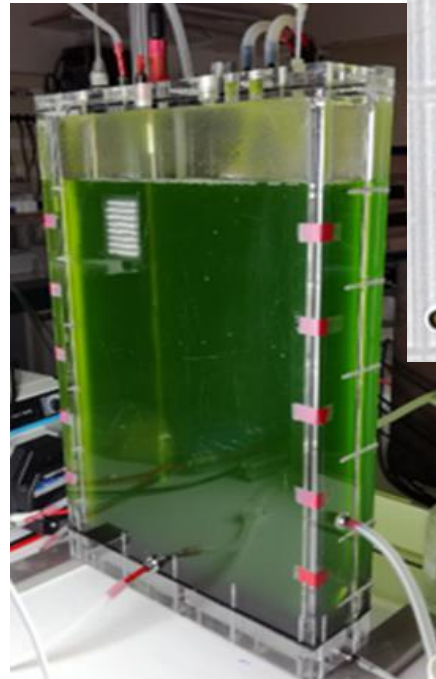
(b) Released TAG

SEQUENTIAL PROCESS, INTEGRATION and ENERGY MINIMUM

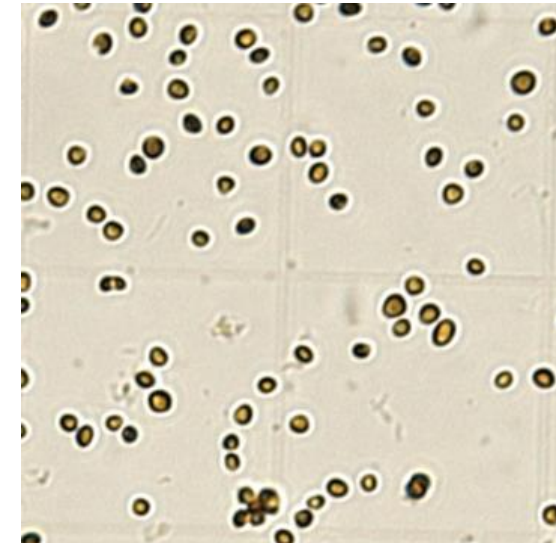
Rosine Zinkoné (2018)

Synchronization of *N. oleoabundans*:

- Cycles de 16h day/ 8h night
- Synchronization **after 4 cycles**



Mother Cells 16h



Daughter Cells 24h

Average of 4 daughter cells /
mother cell

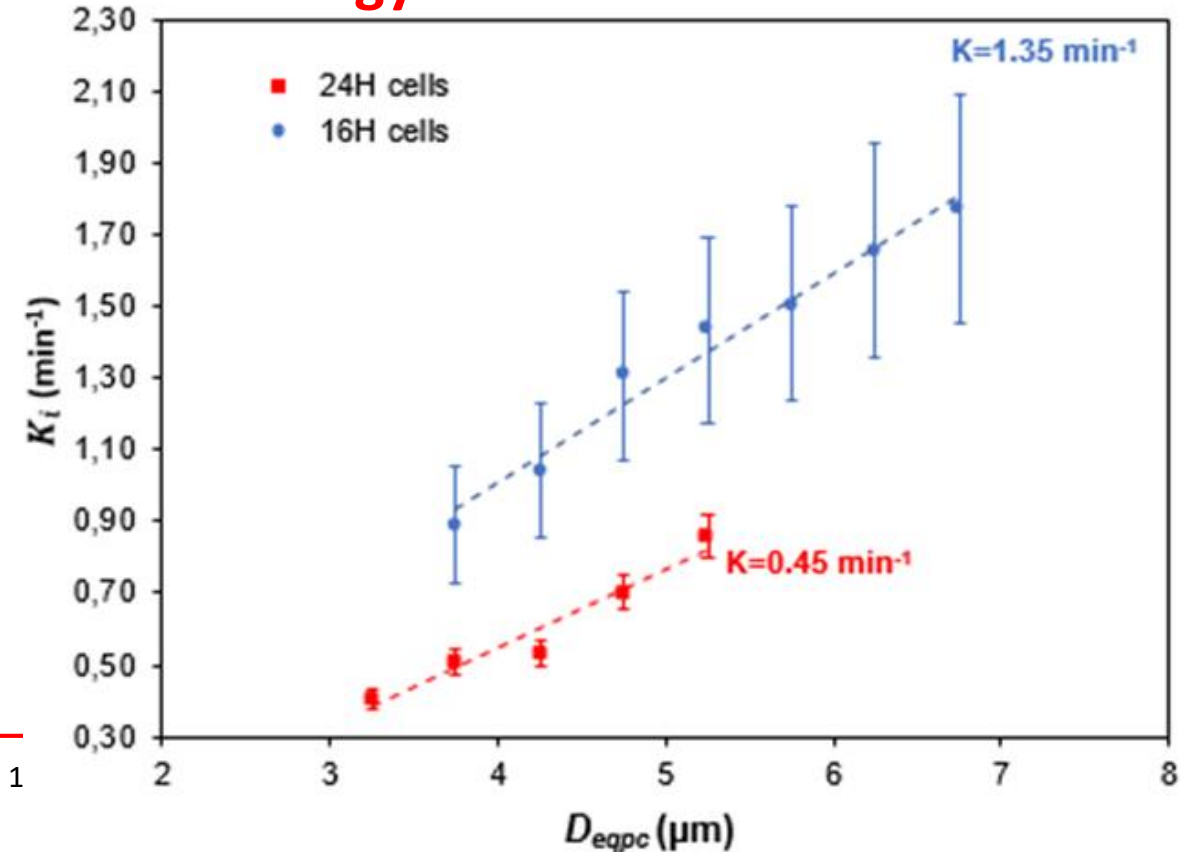
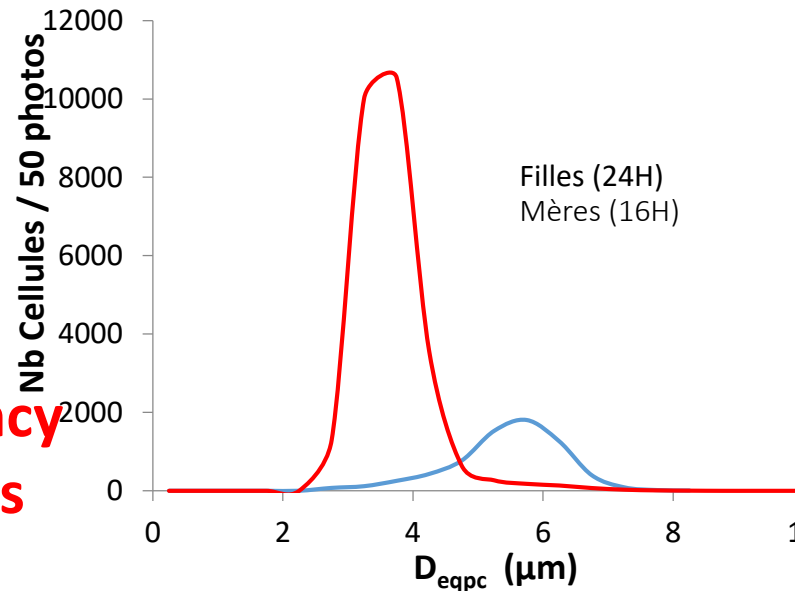
SEQUENTIAL PROCESS, INTEGRATION and ENERGY MINIMUM

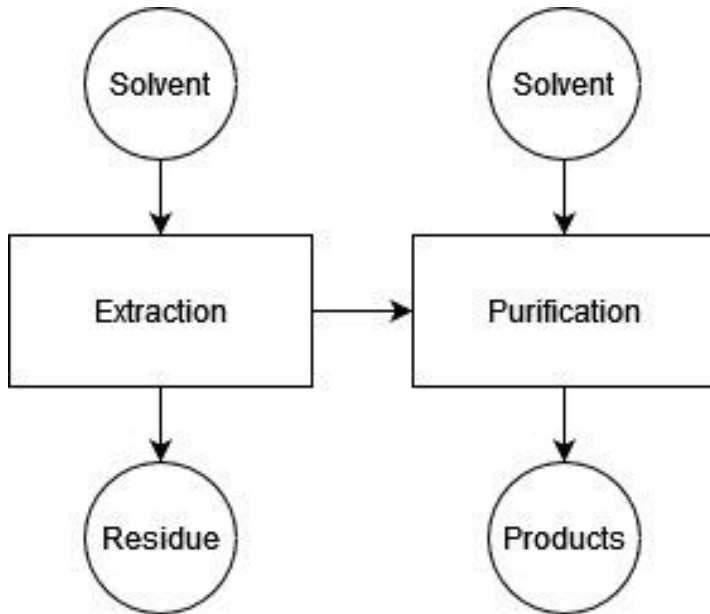
Rosine Zinkoné (2018)

Bead milling kinetics and energy demand

Mother cells are weaker than daughter ones

→ Cell division moment for disruption efficiency and energy savings





→ Extraction and purification with or without solvents ?

→ Solutions for water soluble molecules : **membrane** concentration, fractionation

→ For other metabolites : **what solvents** are in accordance with bioresource valorization ? In accordance with the application field ?

CO₂, green (organic) solvents, NaDES

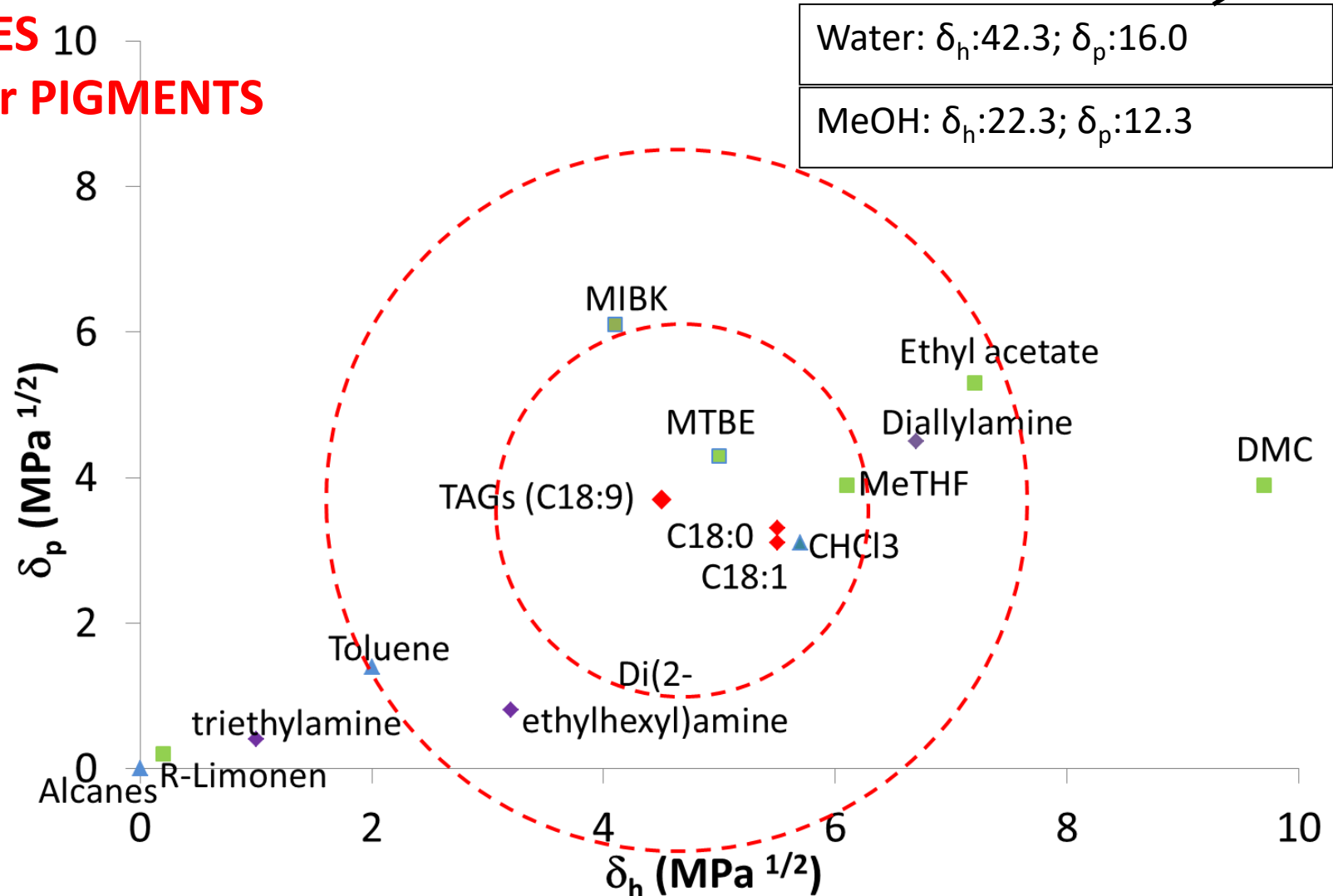
Low volatility phases = des-extraction step ? Carrier solvent ?

→ **Green solvent = green process ?**

SOLVENTS AND TECHNOLOGIES FOR EXTRACTION OF LIPIDS or PIGMENTS

Emilie Angles (2014)

Hansen solubility param.

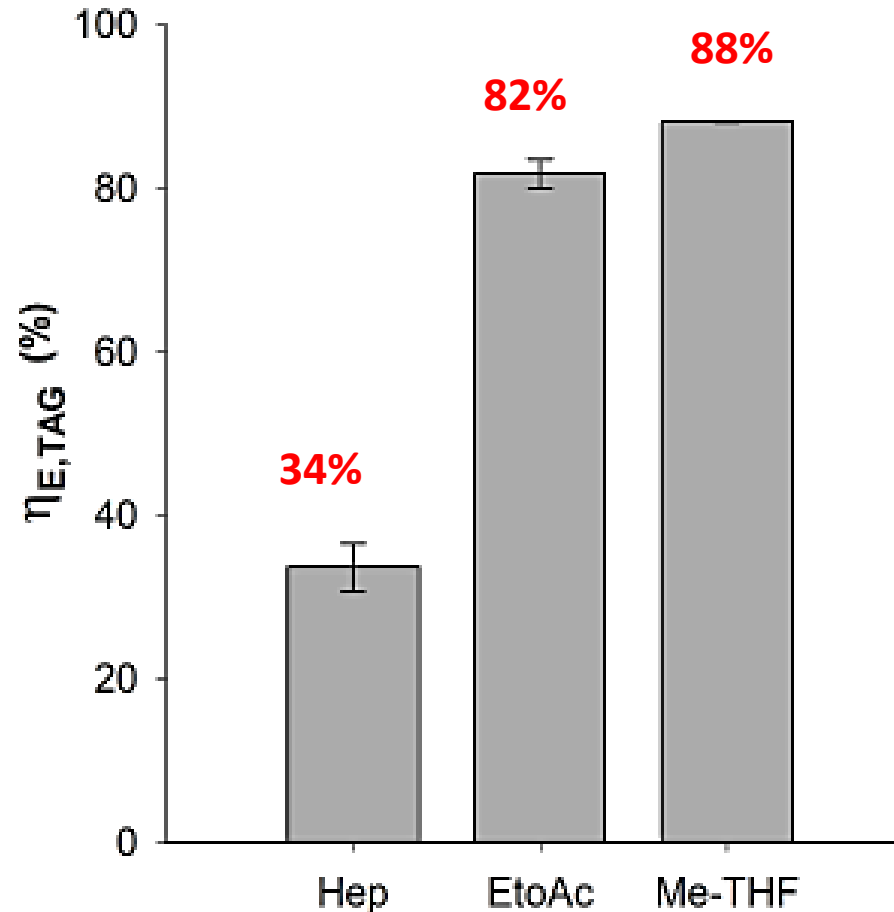


SOLVENTS AND TECHNOLOGIES FOR EXTRACTION OF LIPIDS or PIGMENTS

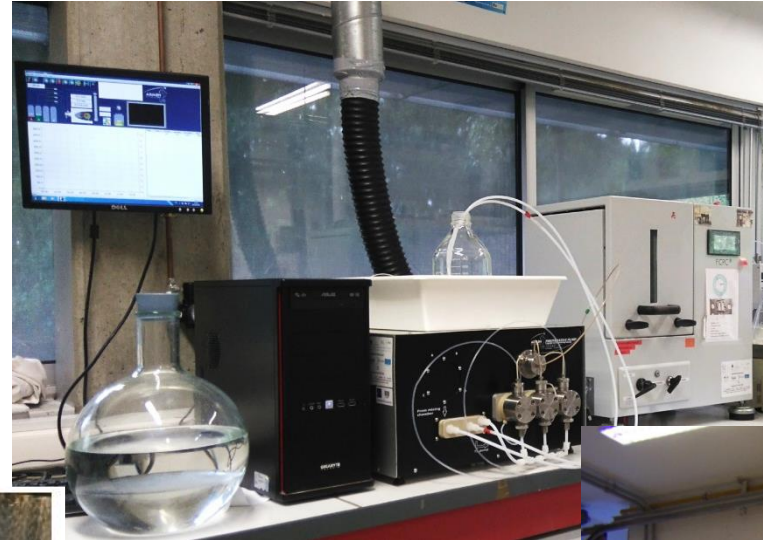
Vladimir Heredia (2020)

Nice performances of lipids extraction in wet route

➔ Solubility with water that make solvent recovery more difficult



SOLVENT CONSUMPTION REDUCTION (PROCESS INTENSIFICATION by CENTRIFUGATION)



CPC



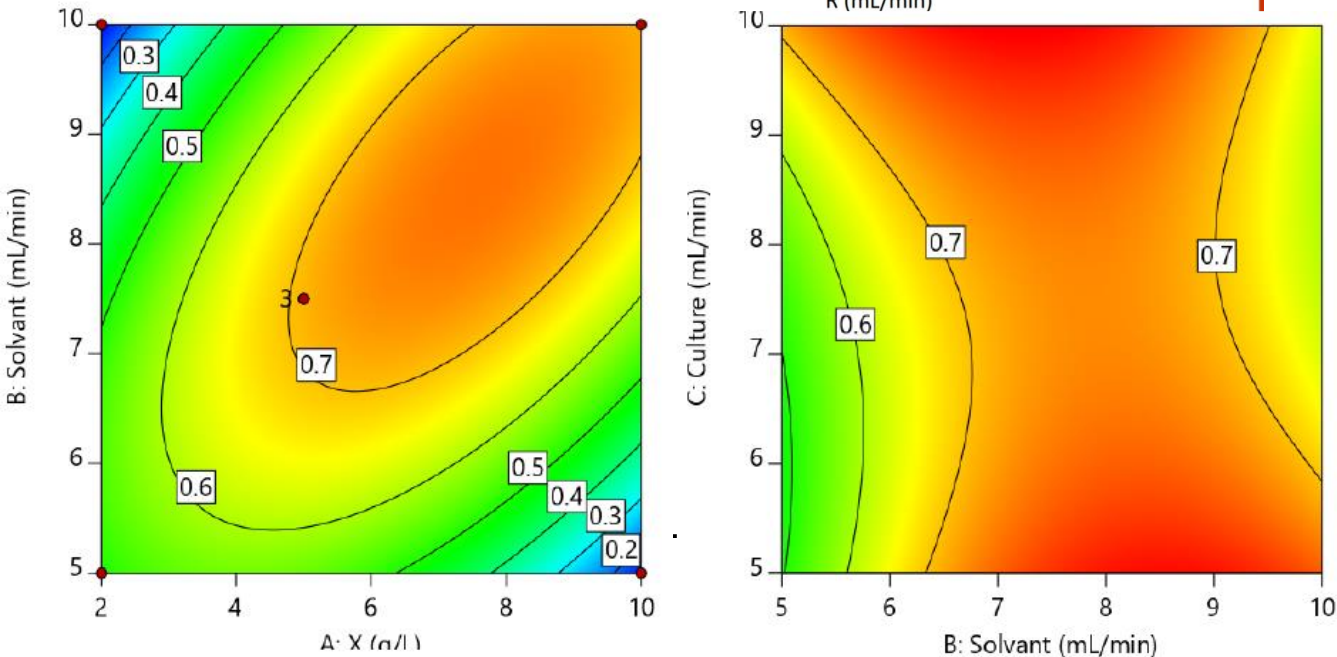
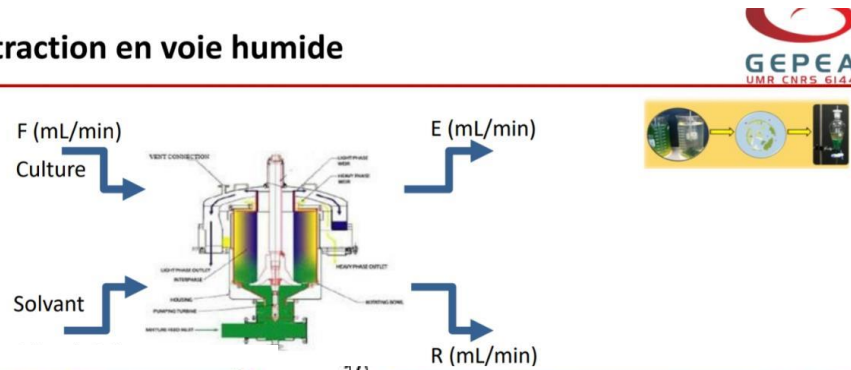
BXP



BXP : one stage, continuous

Optimisation de l'extraction en voie humide

• Resultat Preliminaires

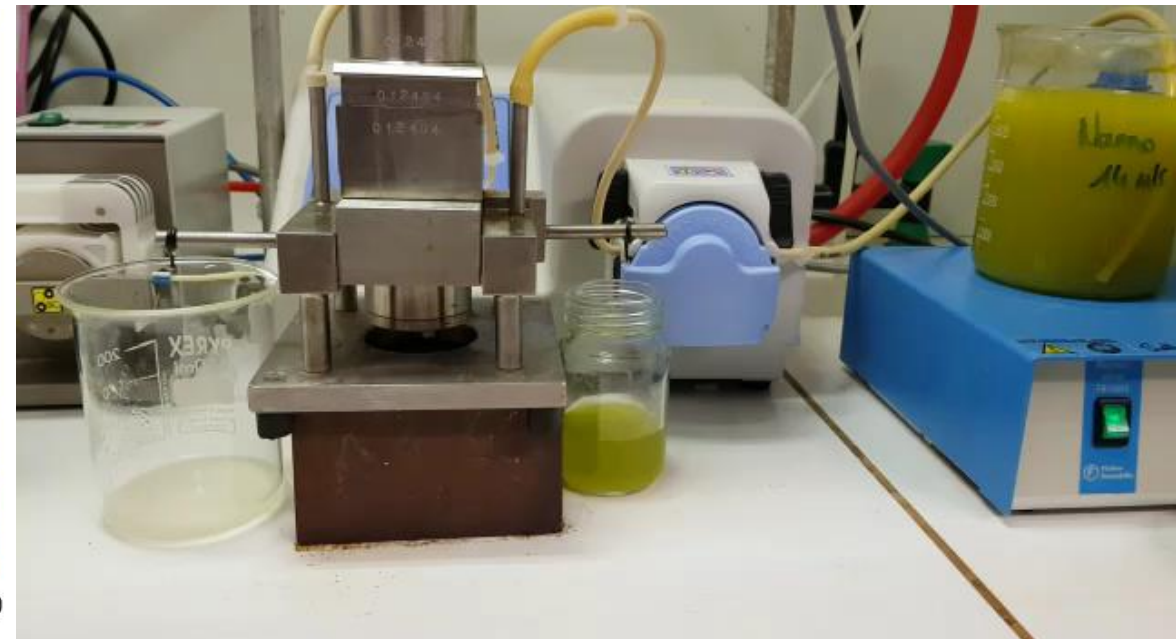


Extraction yields: 75-80%

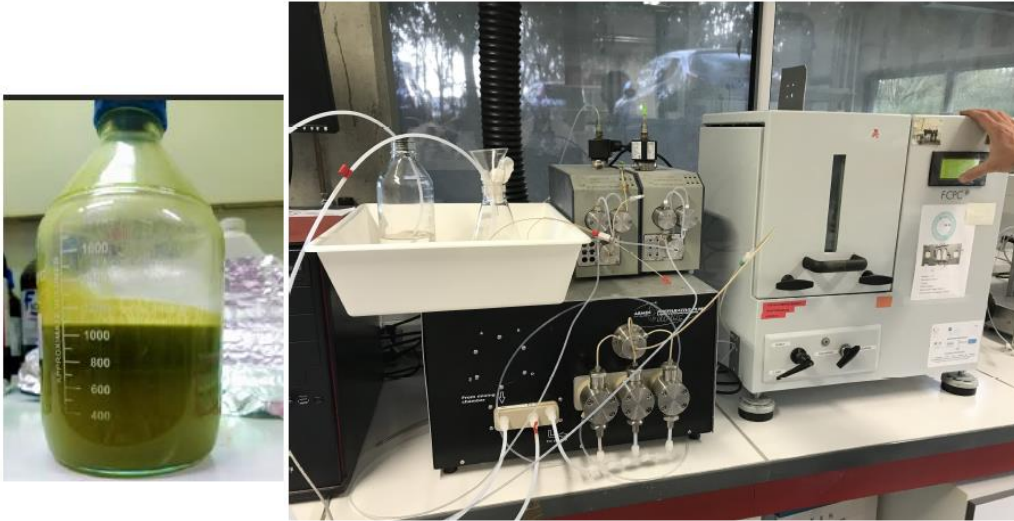
Limitations:

Low dw concentrations at process inlet (5-6 g/l) Optimal Solvent Ratio : **1**

Specific solvent need 172 g/g_{ms}



CPC : one stage, discontinuous



Extraction yields: >80%

Limitations:

Low dw concentrations at process inlet (5-6 g/l) Optimal Solvent Ratio : **0.07**

Specific solvent need 23 g/g_{ms}



Green solvents can be implemented

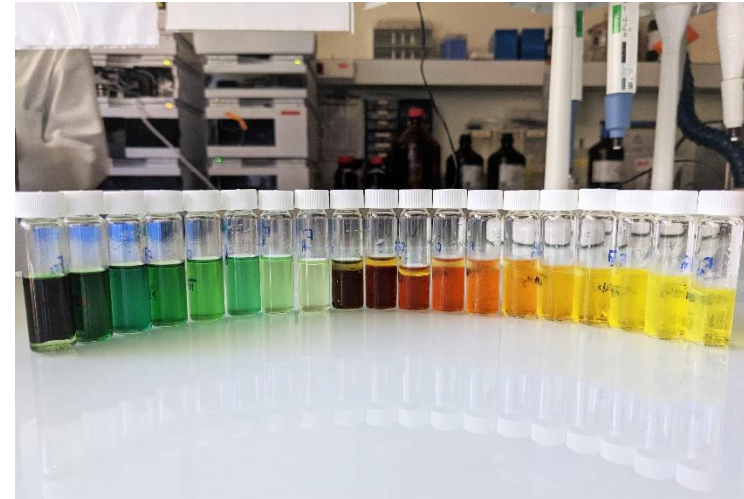
8x Solvent reduction by technology

➔ Still some limitations

	Heptane	m-THF
Density	0,68	0,86
Bp (°C)	98,4	79,0
Solubility in water	3,4 mg/l	130 g/l (décroit avec la T)
lipids recovery	80 %	150 %
TAG recovery	35 %	83 %

CONCLUSIONS :

- Microalgae can have a growing production cycle controlled by solar day/night cycle
- This has a direct effect on microalgae composition, size and mechanical robustness
- Some strategy for optimal metabolite release and disruption energy minimization can be proposed for sequential production
- Membrane concentration, fractionation is efficient for biopolymers, hydrolysates
- For lipids, alternative (green) solvents can be proposed for extraction or purification
- For low volatility solvents (glyOH, oils, NaDES): solvent recycling issues



THANK YOU FOR YOUR ATTENTION
SEE YOU SOON in SAINT NAZAIRE !

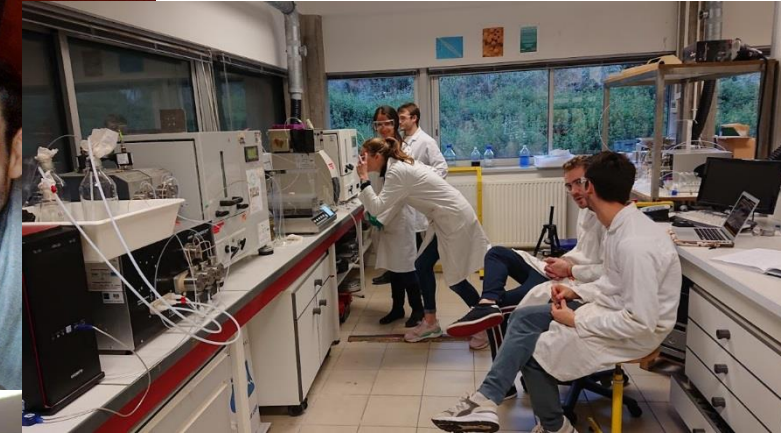


ENHANCE
MICROALGAE

Interreg
Atlantic Area
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EUROPEAN UNION



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